



**SAWEA Workshop, 2005**

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# **ZeeWeed MBR Technology Update**

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ZENON Environmental Inc**

# Presentation Outline

- ZeeWeed® MBR Technology
- ZENON MBR Technology Update
- New ZENON Projects
- Q & A

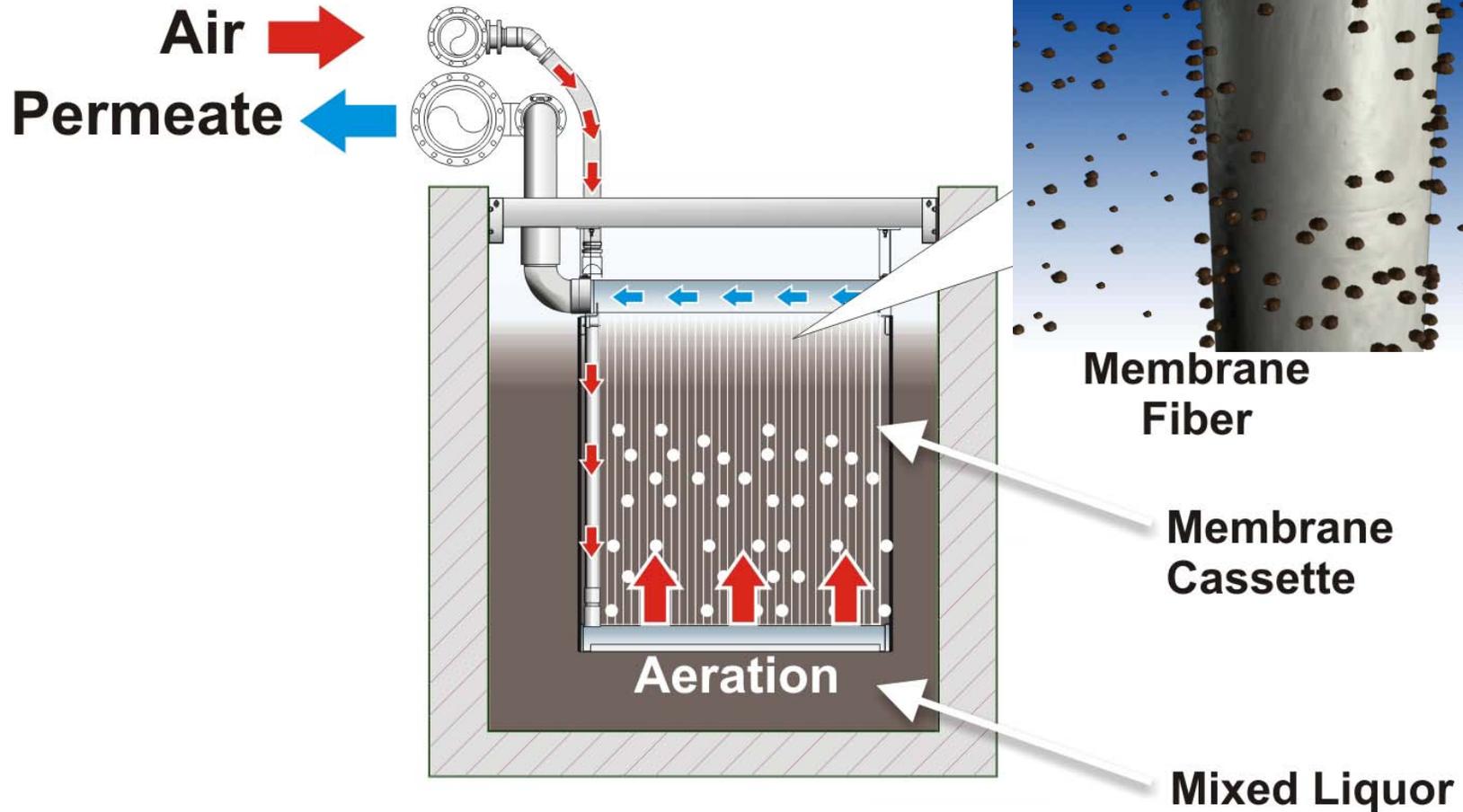


# ZeeWeed<sup>®</sup> MBR Technology

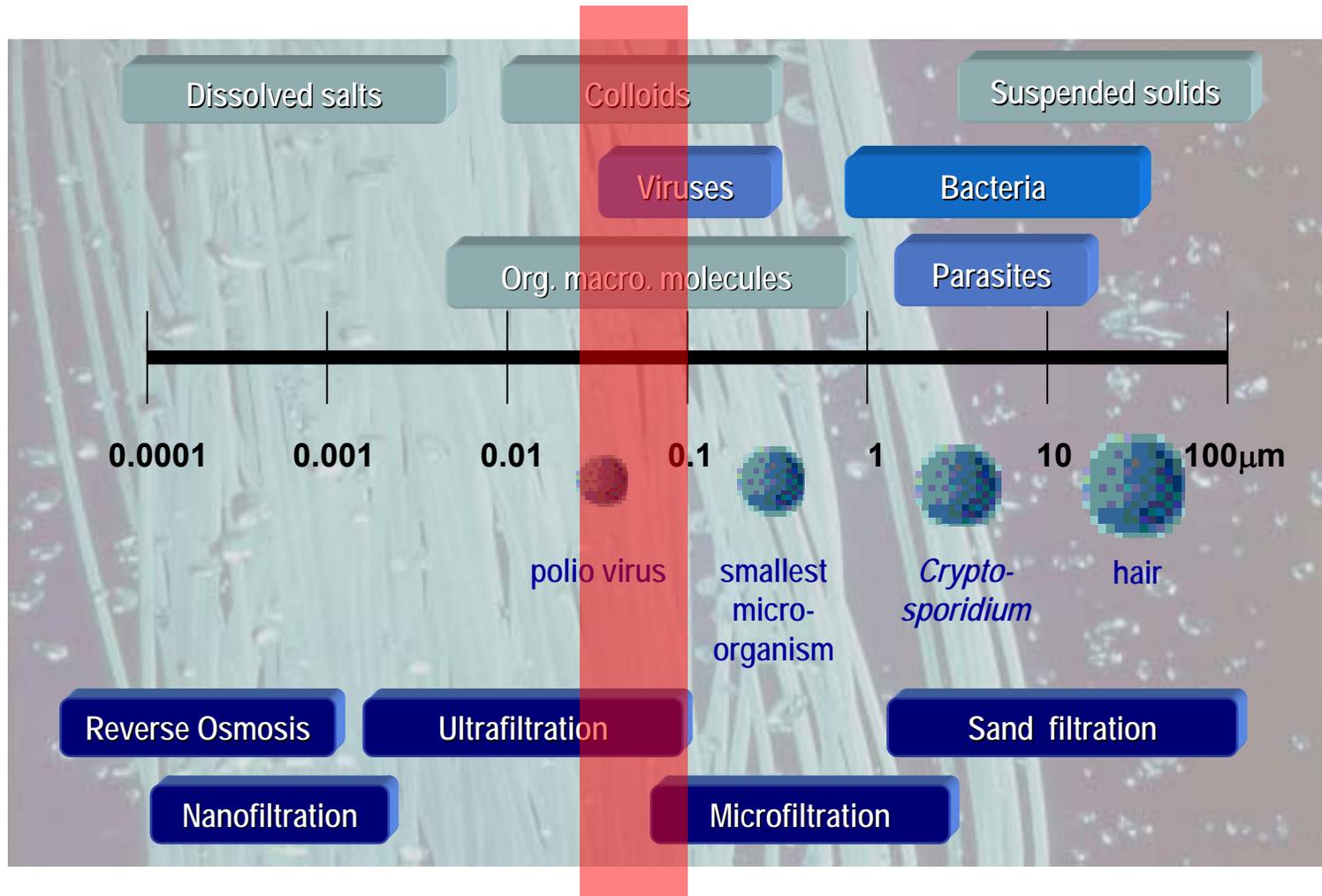
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# Principles of ZeeWeed<sup>®</sup> Immersed Membranes



# Membrane Filtration



ZENON membrane range

# ZeeWeed® 500 – Robust Membrane

- Reinforced for maximum strength and maximum life
- Failure proof / double barrier
- High solids tolerance



# ZeeWeed<sup>®</sup> Cassette Scale-Up

Larger Plants = Larger Cassettes

ZW-500a (1997)



4,000 ft<sup>2</sup>  
80,000 gpd

ZW-500c (2000)



5,500 ft<sup>2</sup>  
110,000 gpd

ZW-500d (2002)



16,300 ft<sup>2</sup>  
326,000 gpd

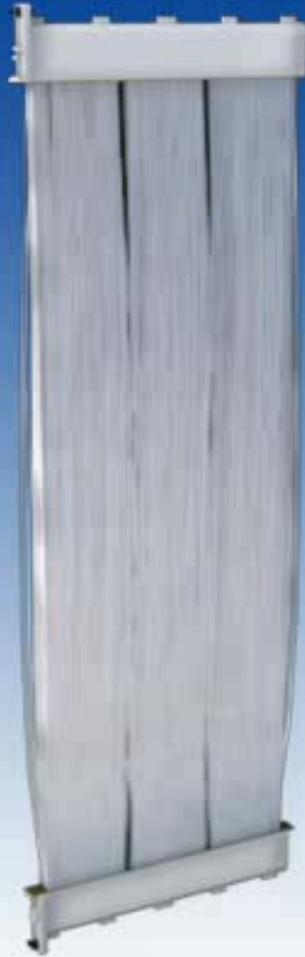


# ZeeWeed<sup>®</sup> 500d – Cassette

## Optimized Building Block

- **Compact**
  - High packing density = small footprint
  - Low energy costs
- **Accessible**
  - Easy to remove modules and cassettes
- **Simple**
  - Fewer connections, valves = higher reliability
  - Lower capital costs

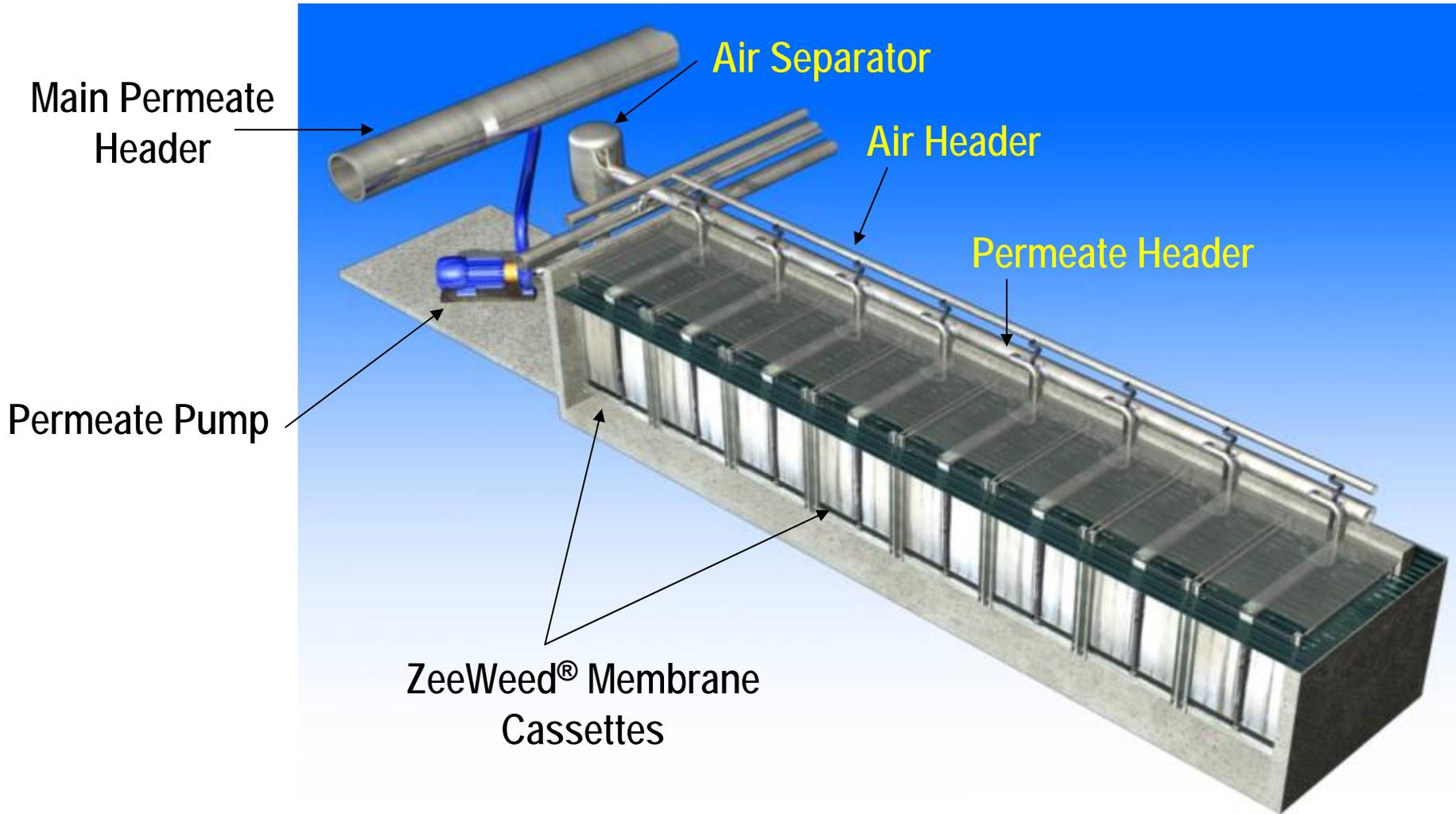




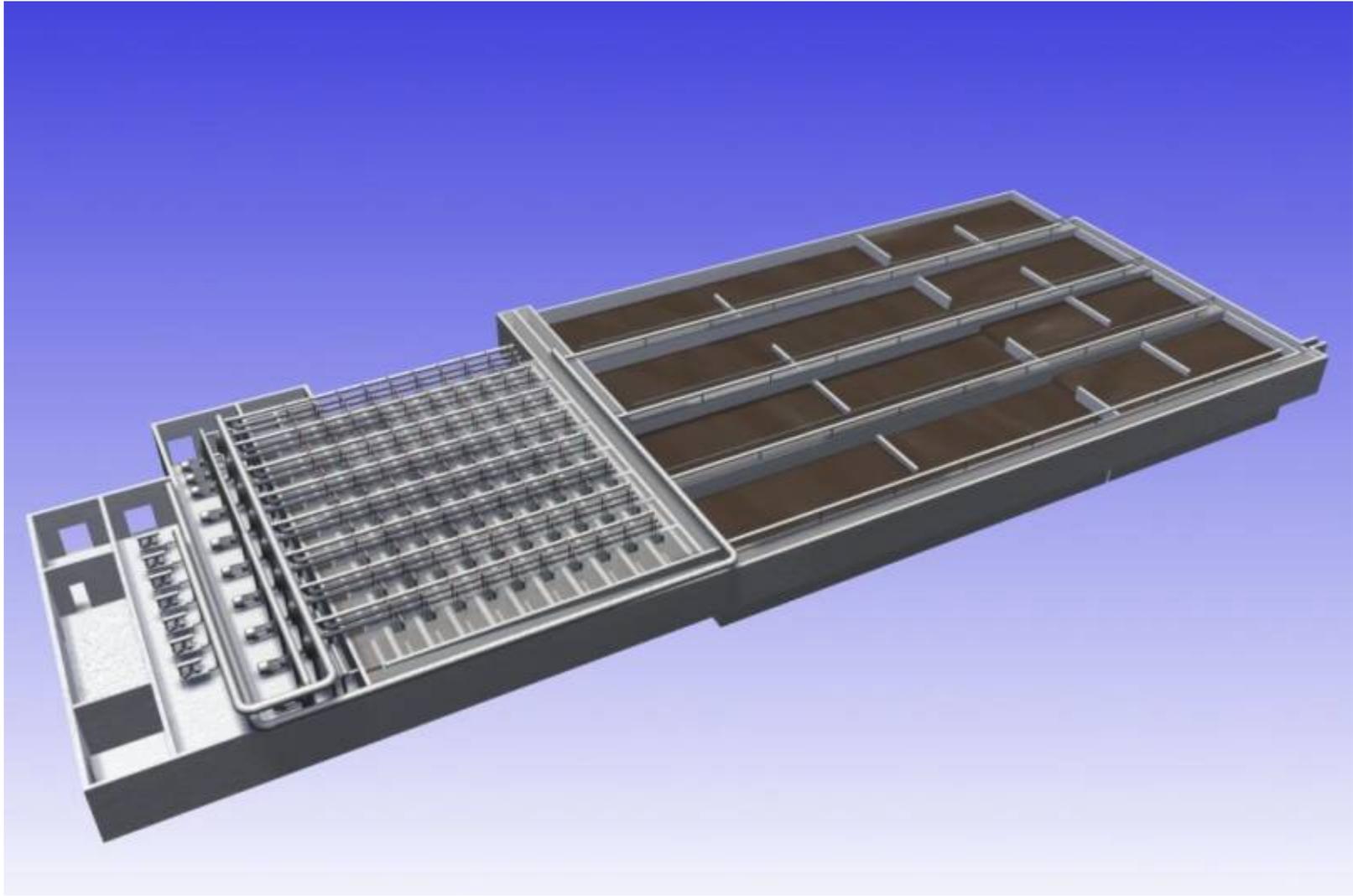
Water for the World

© 2003 ZENON Environmental Inc

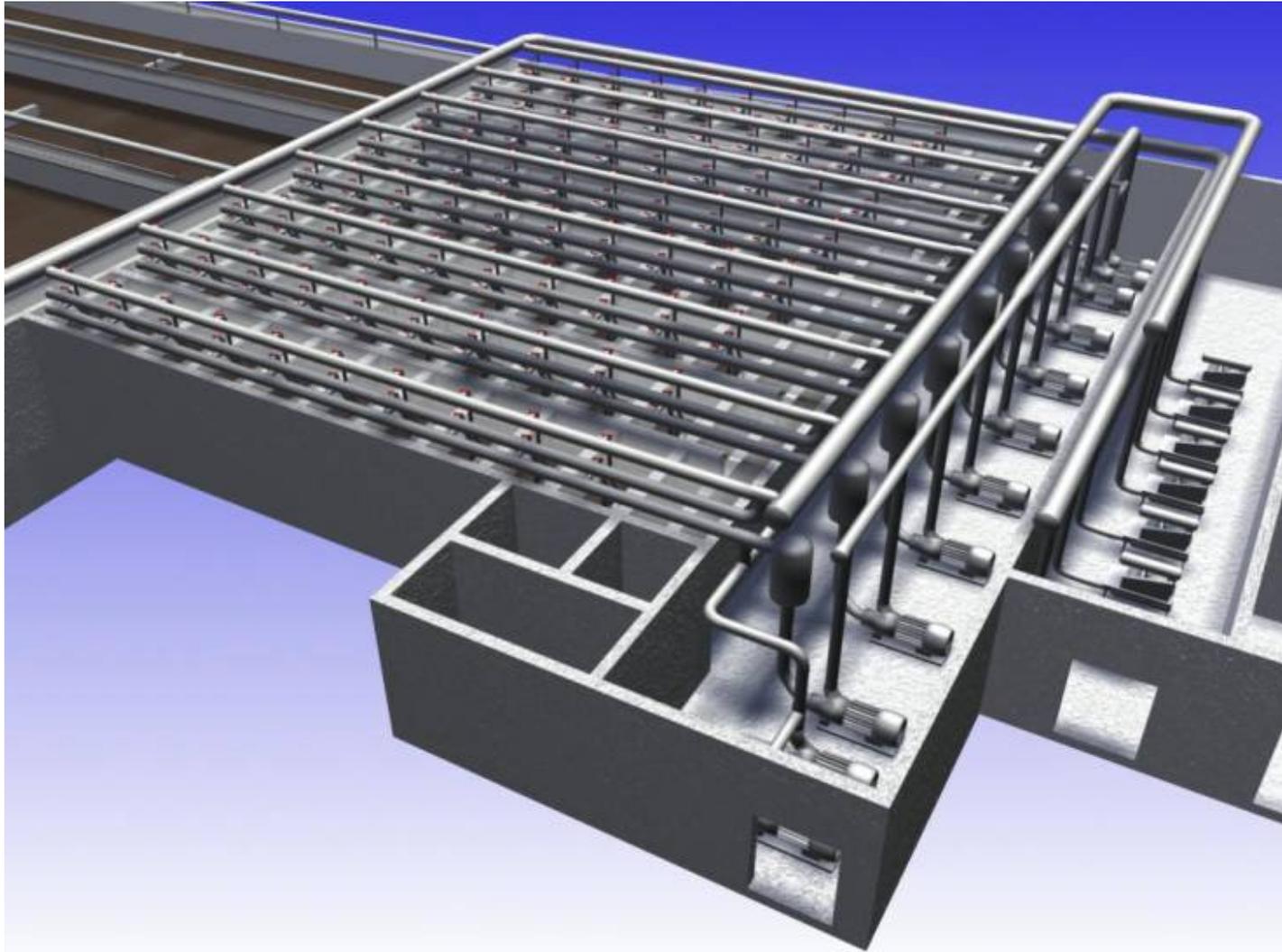
# ZeeWeed<sup>®</sup> 500d – Train



# Overall ZeeWeed<sup>®</sup> MBR Design



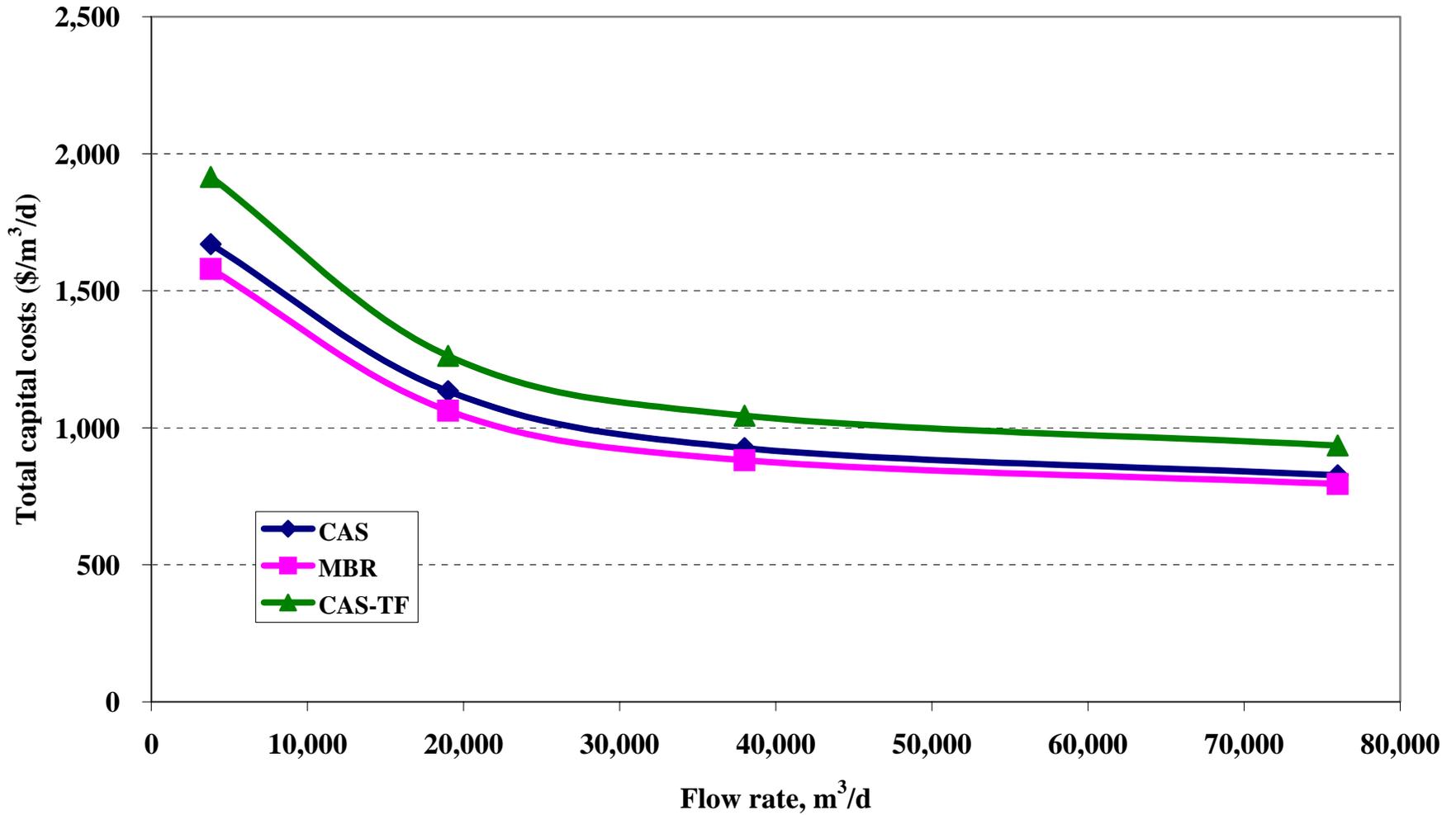
# Simple, Modular ZeeWeed<sup>®</sup> Design



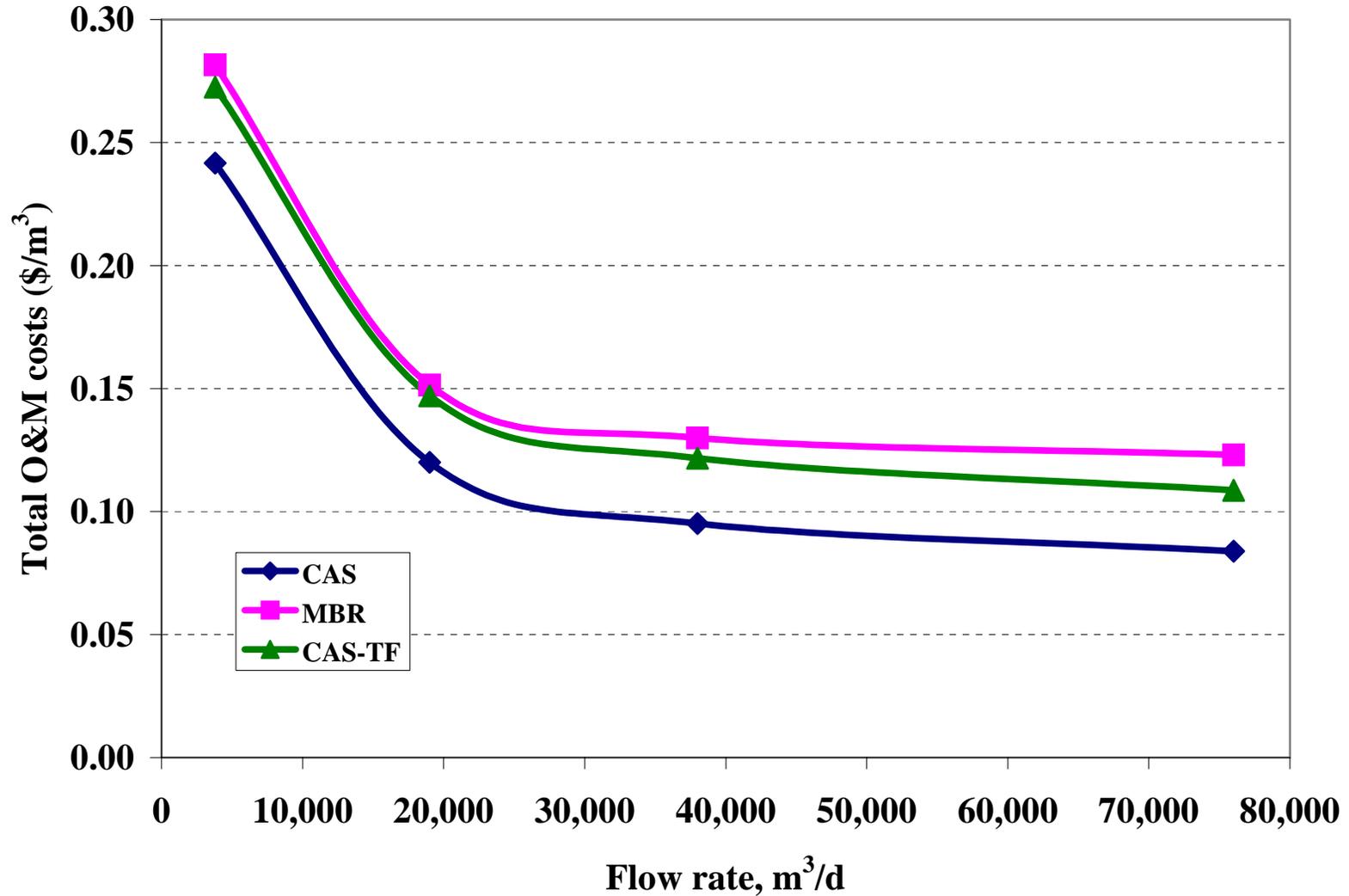
# ZW MBR Technical Update

1. Drivers for Change - Efficiency
2. Effective Pre-Treatment
3. Simplified System Design
4. Comprehensive Cleaning Toolbox
5. Optimized Life Cycle Costs - Energy
6. Membrane Life and Warranty
7. Chemical Conditioning

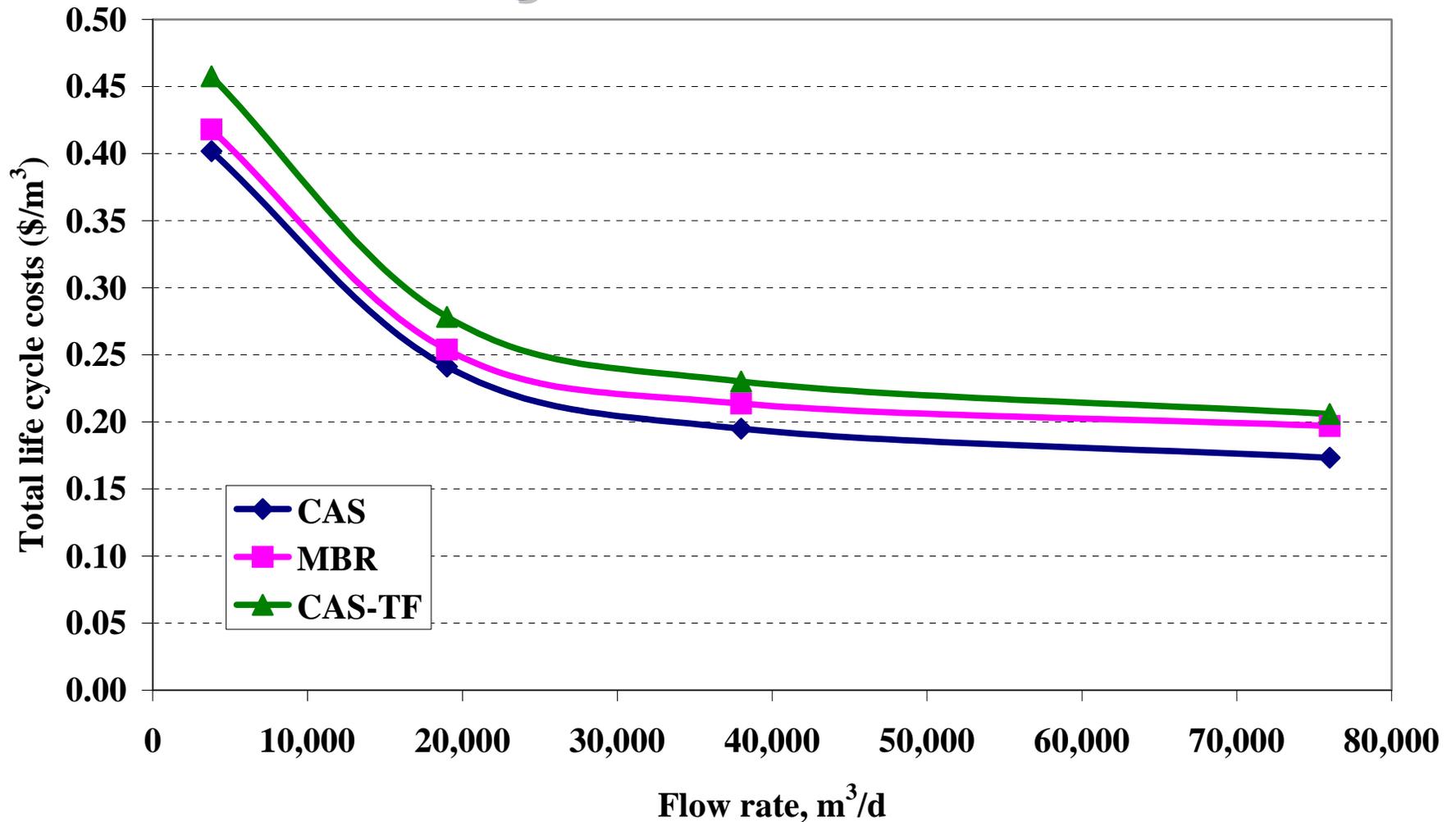
# Total Capital Costs



# Total O&M Costs



# Total Life-Cycle Costs



# Pre Screening Experience & Recommendation

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# Hollow Fibre



# Flat Sheet



# Acceptable Screen Types

- Internally-fed rotary drum screen
- In-channel rotary drum screen
- Rotating brush screen
- Travelling band screen

# Screening Requirement

- **$\leq 2$  mm mesh or punched hole, with no possibility of screenings carry-over or bypass**
- **Preferred:  $\leq 1$  mm mesh or punched hole screening**
- European market is well on the way to acceptance of  $\leq 1$  mm screens

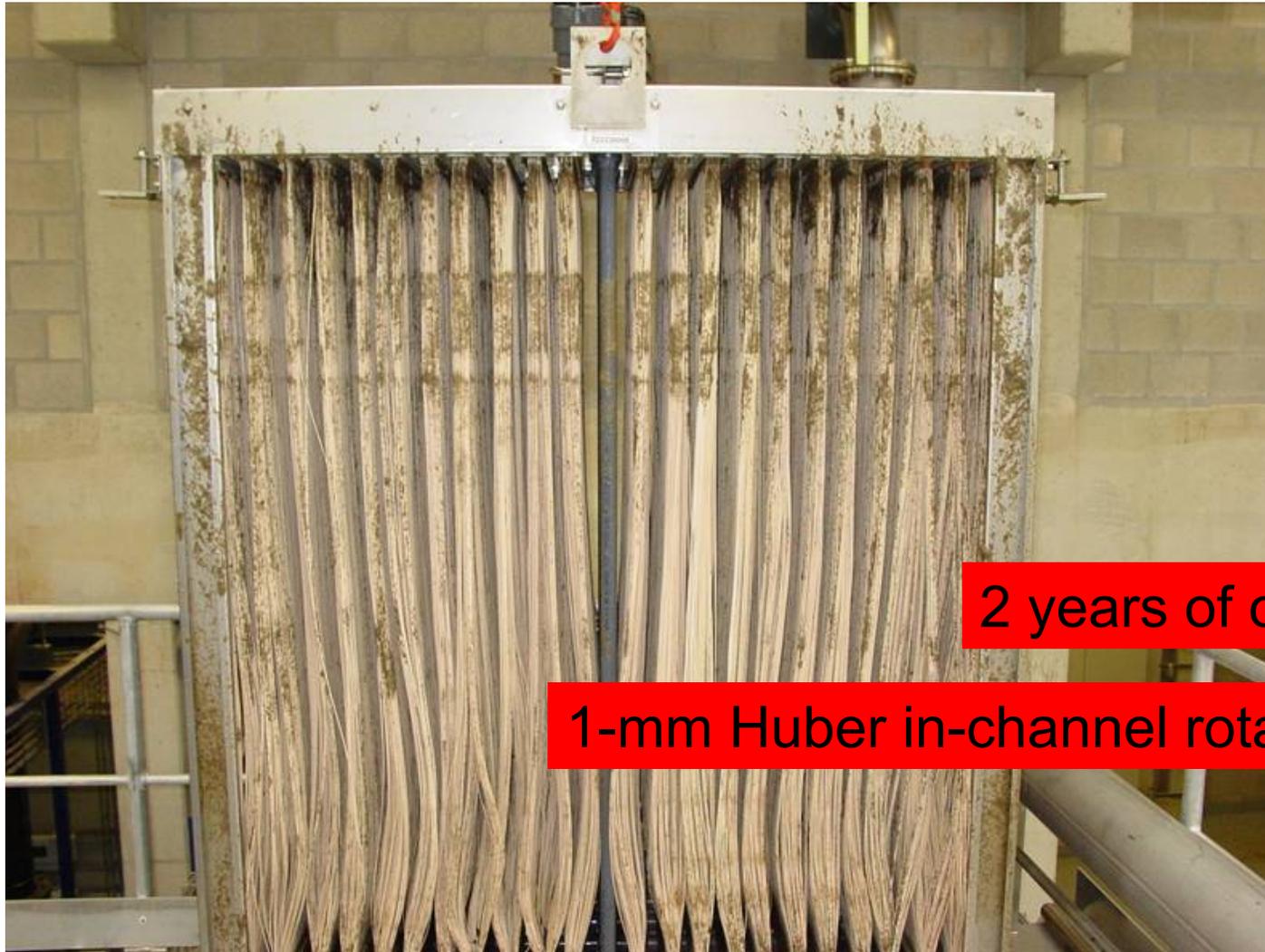
# Brescia, Italy



2.5 years of operation

2-mm Huber in-channel rotary drum

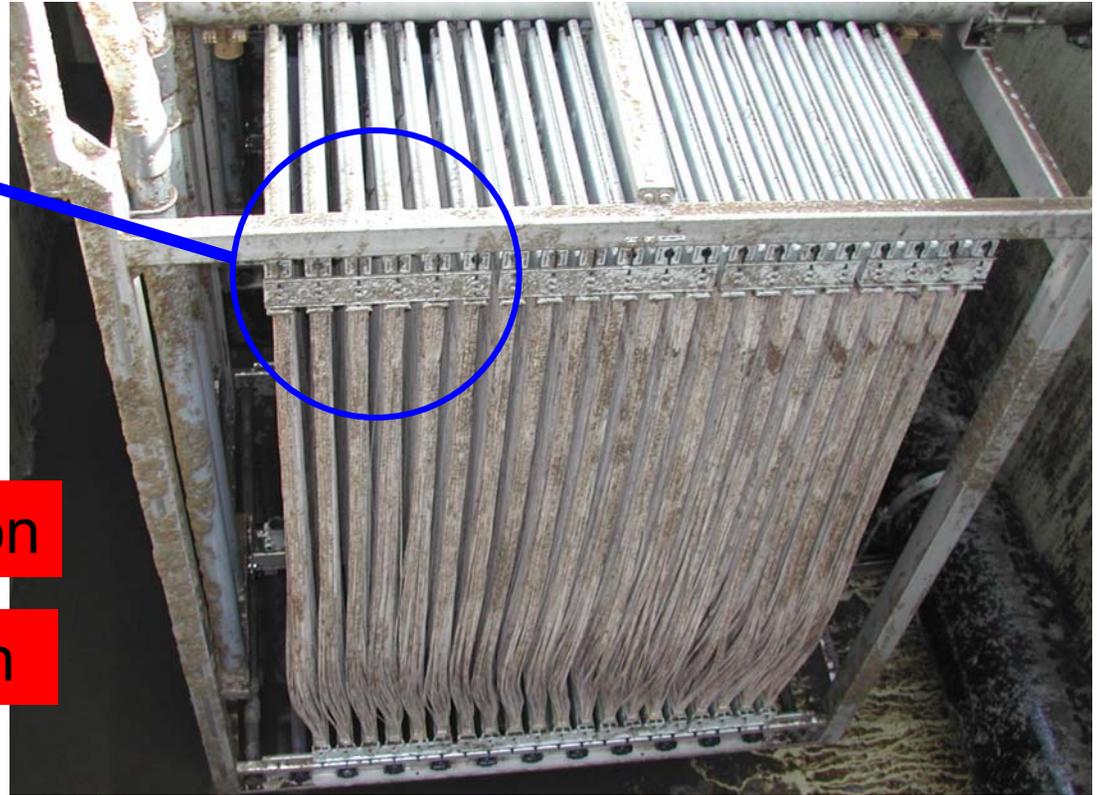
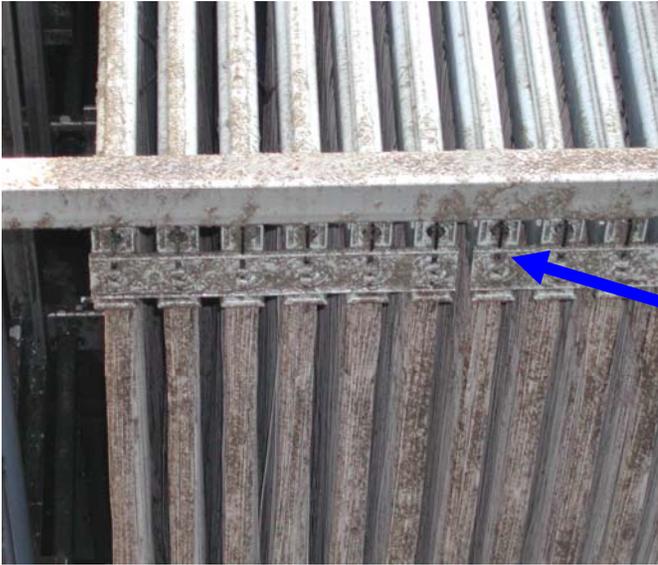
# Schilde, Belgium



2 years of operation

1-mm Huber in-channel rotary drum

# Varsseveld, Netherlands



5 months of operation

0.8-mm rotating brush

# Benefits of Fine Screening

- Higher sustainable flux
- Longer membrane life
- Longer cleaning intervals
- Less equipment maintenance
- Insurance: protection of most valuable asset!

# Membrane Filtration System Design

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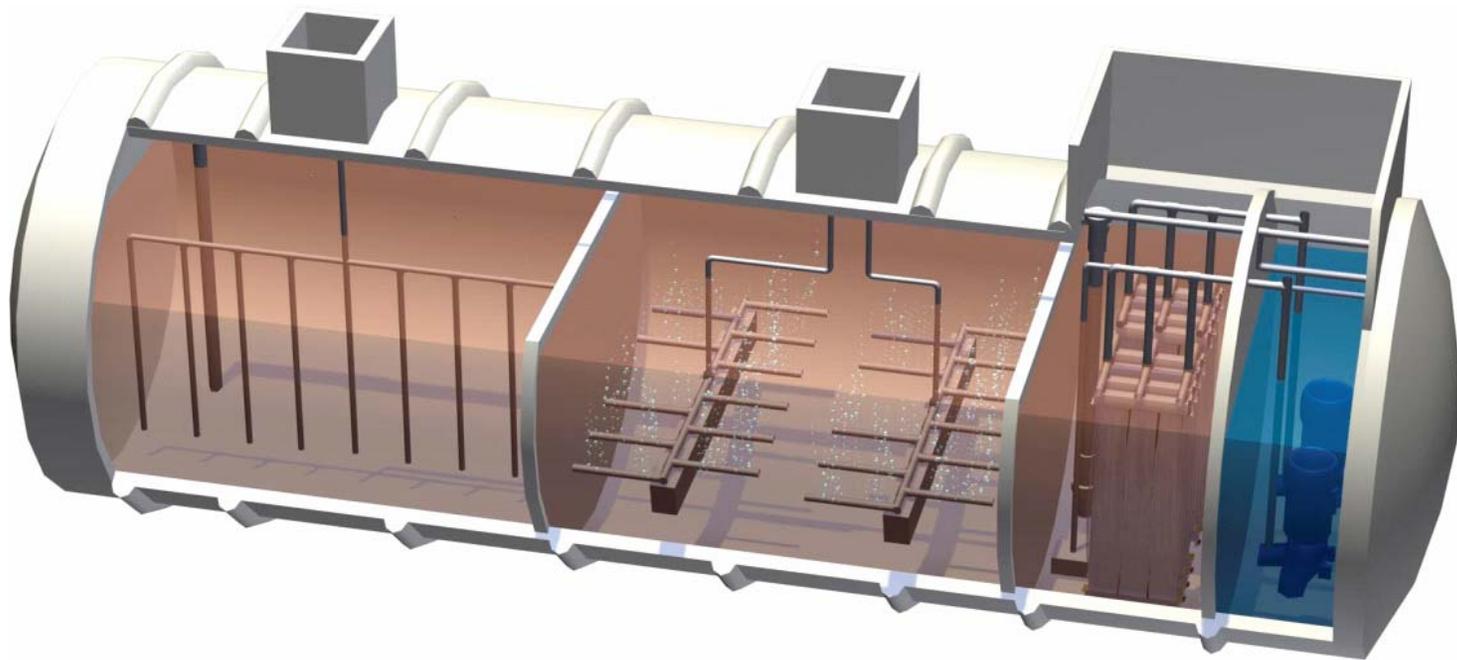


# Filtration Package Plants

- Standard MWW units
- ZENON Standard components
- Cost savings due to pre-engineering



# Full Scope Package Plants



# Custom Membrane System Design

- Reversible pumps
- Removal of air separator
- Siphon designs
- Redundancy

# Not So Simple Design

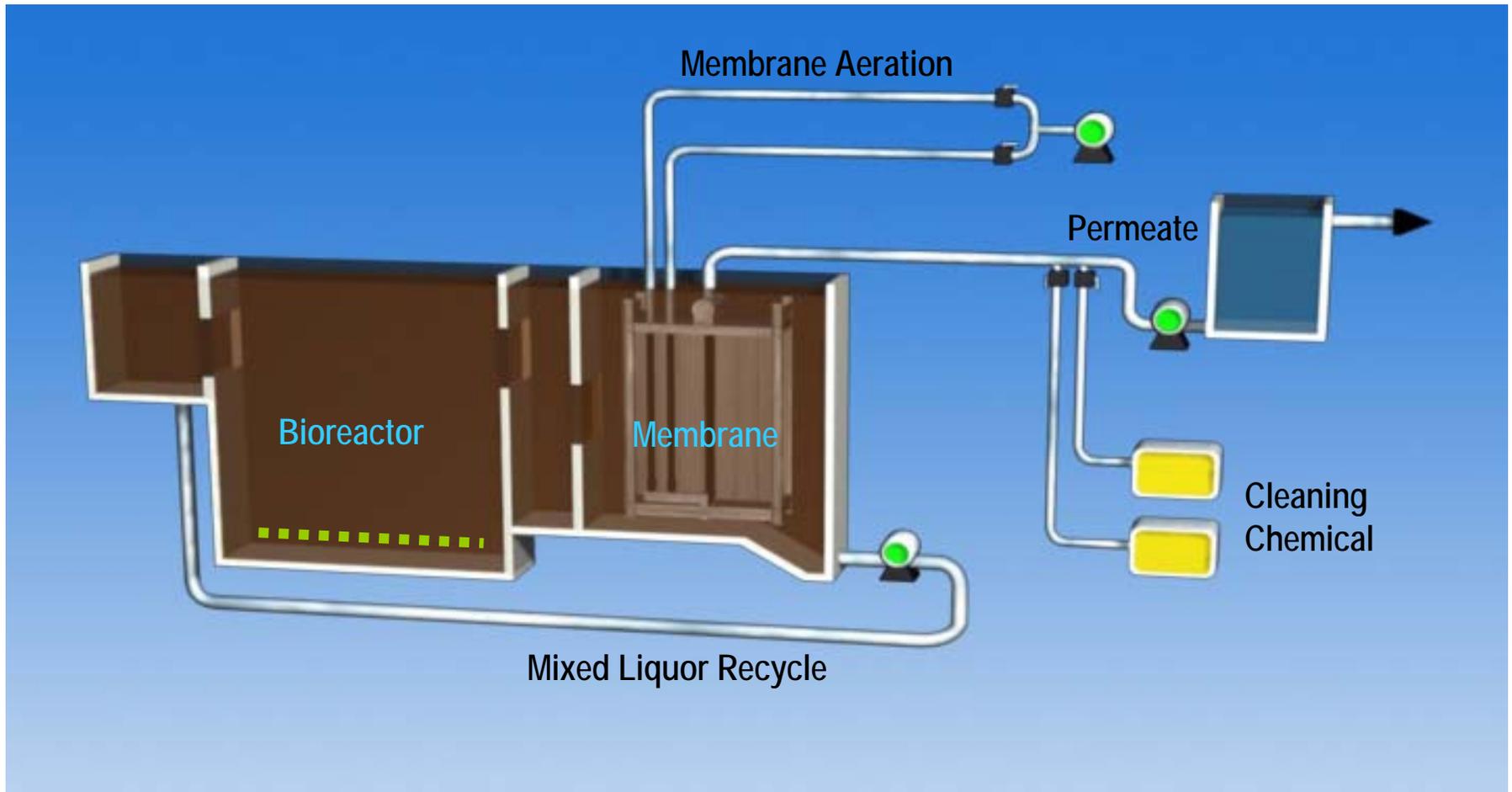
## Creemore



## Cauley Creek



# Simple Design – Reversible Pump



# Simple Design using Reversible Pumps

## Woodstock



## NordKanal



# Permeate by Gravity / Siphon

- **ZENON uses a Controlled Siphon – control valve**
- **25 ft minimum head**
- **ZeeWeed<sup>®</sup> MBR plants**
  - Lowestof, UK
  - Buxton, UK - **4.4 mgd**
  - Linwood, GA – 7 mgd under design



# Membrane Cleaning

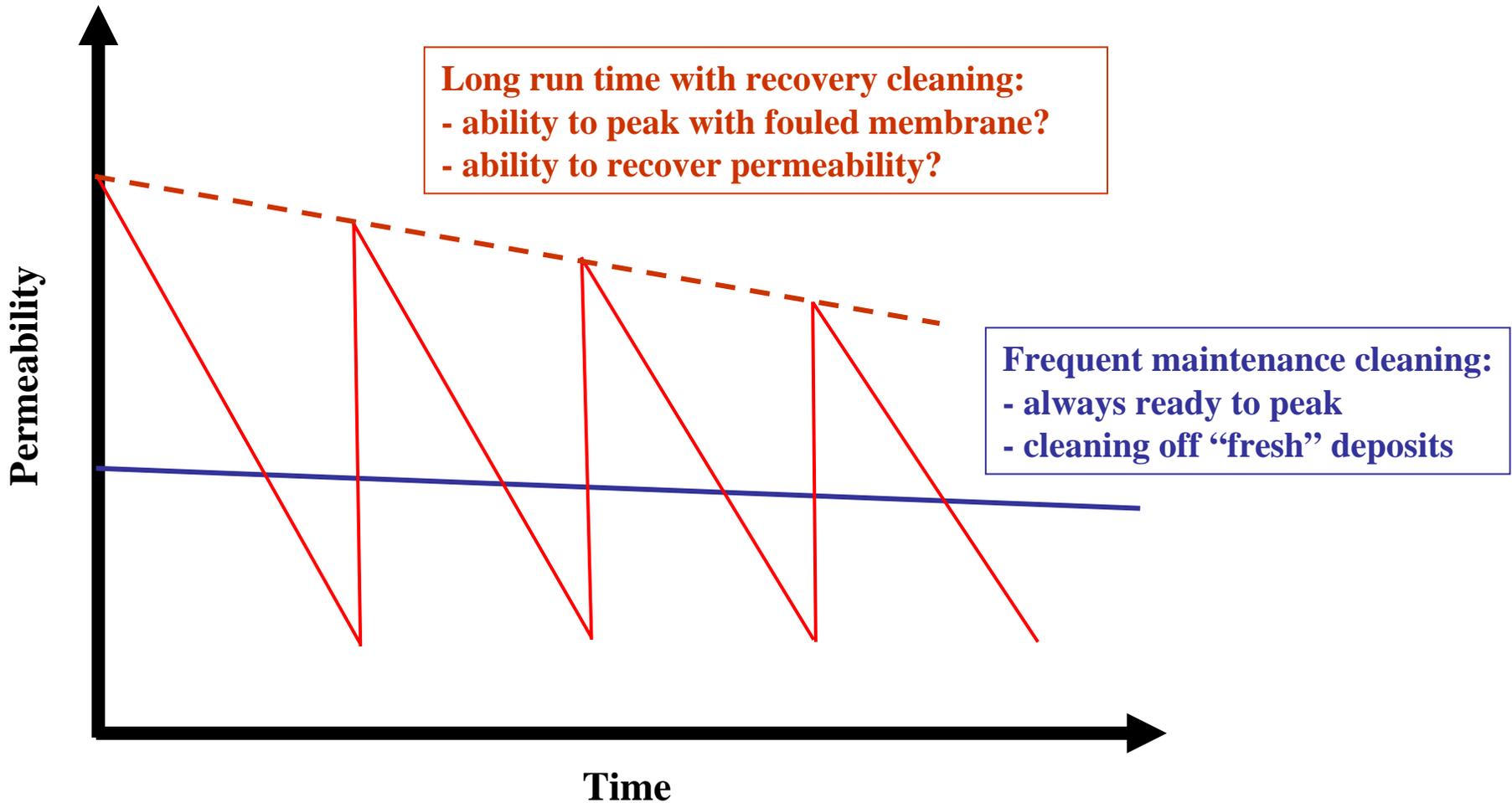
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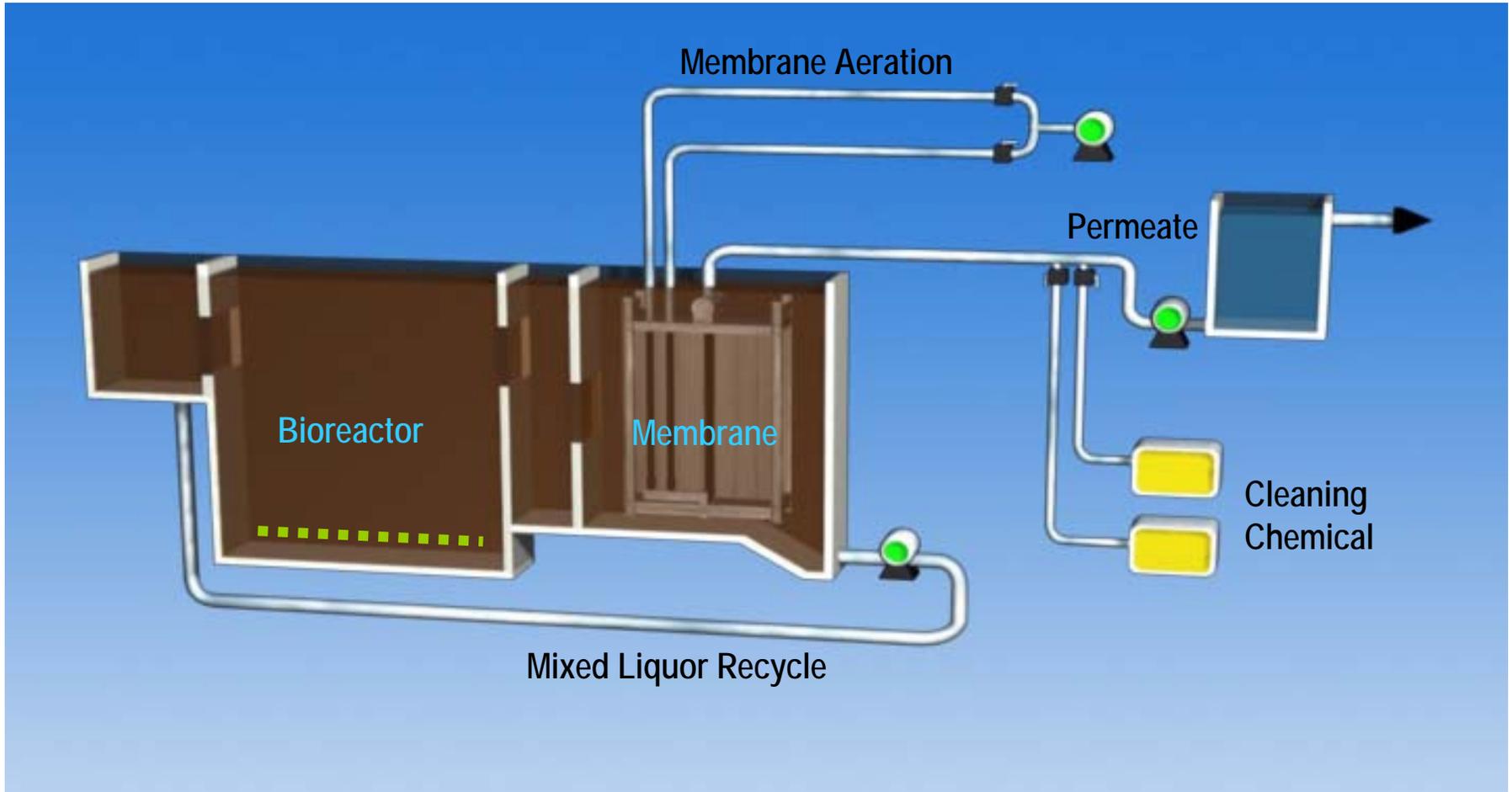
# ZENON Cleaning Toolbox

- In-situ membrane cleaning
  - Reduce handling of membranes
- Fully automated cleaning procedure
  - Reduce operator requirements
- Regular, less intense cleaning
  - Maintain a higher membrane permeability
- Backpulse cleaning chemicals
  - Improved cleaning effectiveness

# MBR Operation Philosophies



# Automated Membrane Cleaning

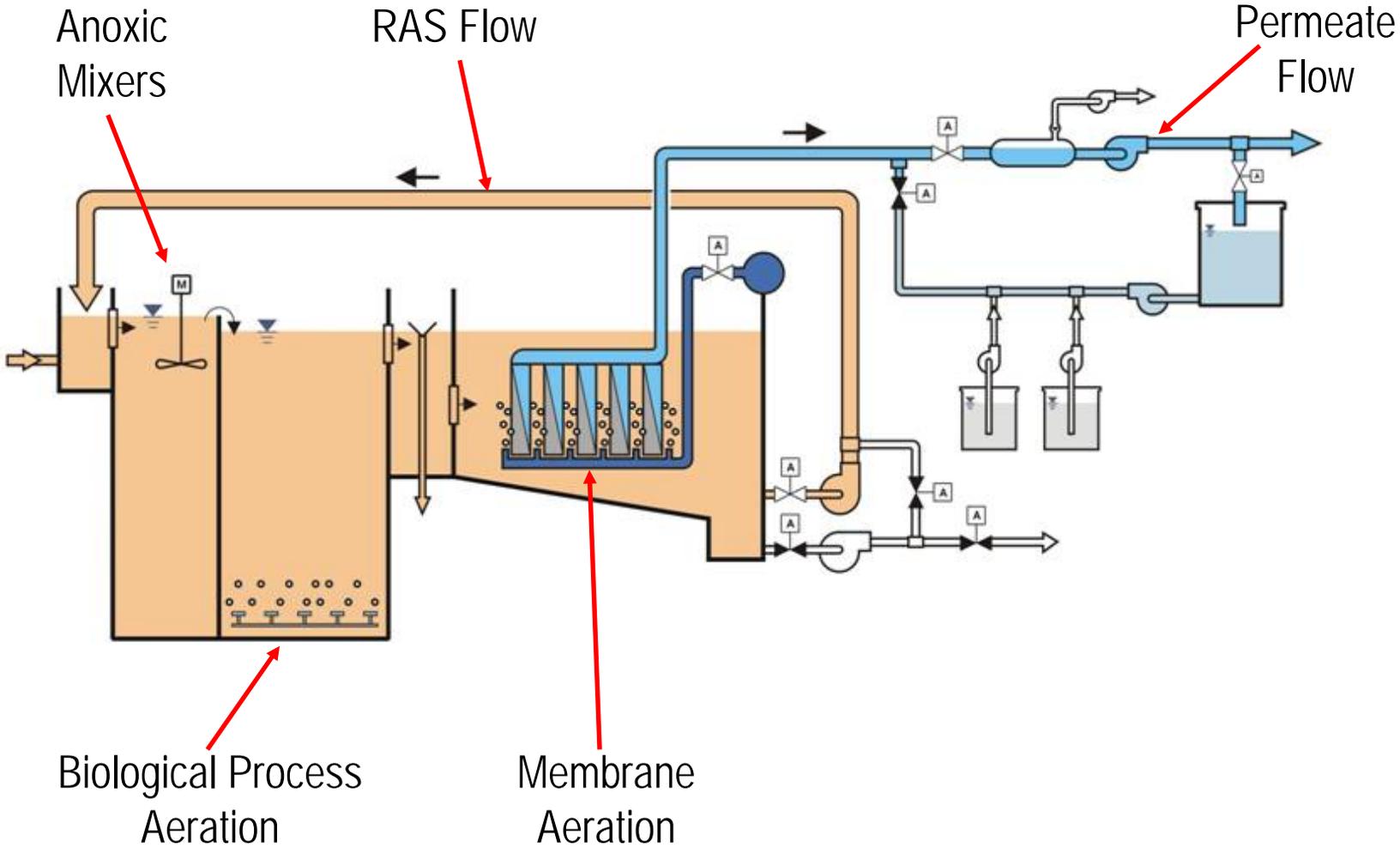


# Energy Optimization

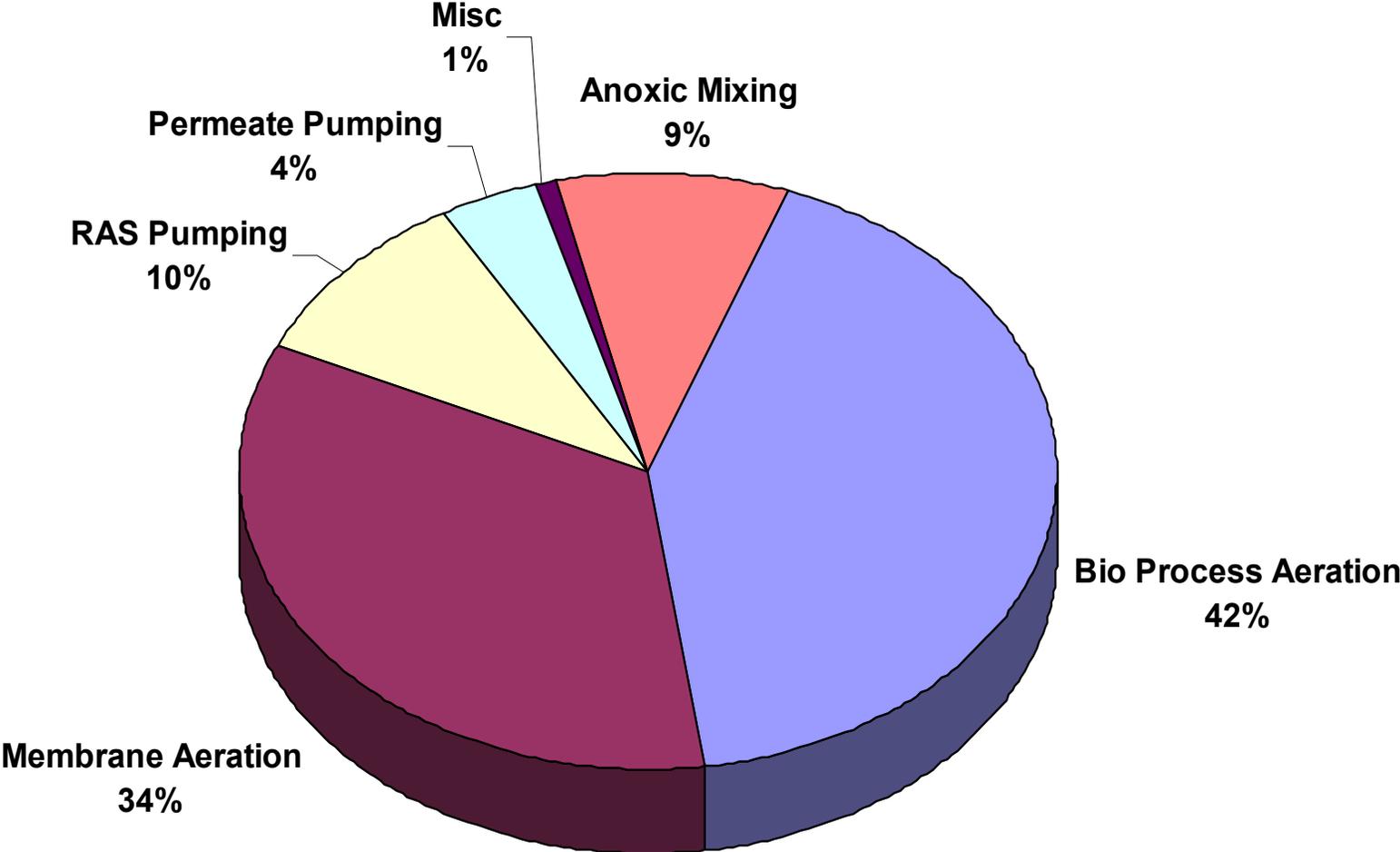
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# MBR Energy Users



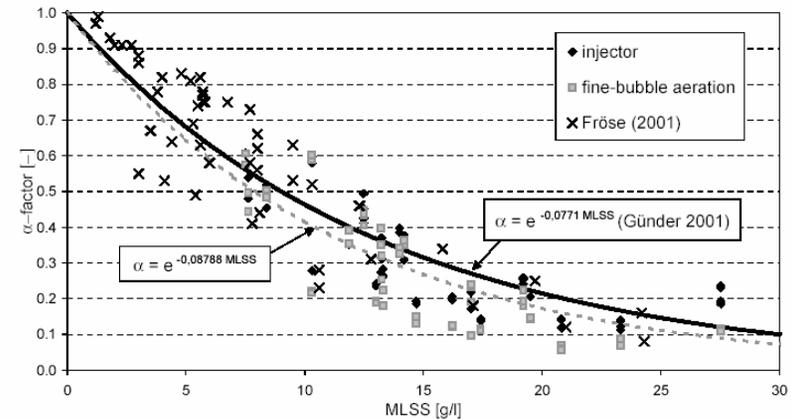
# MBR Energy Users



# Optimizing Energy Efficiency

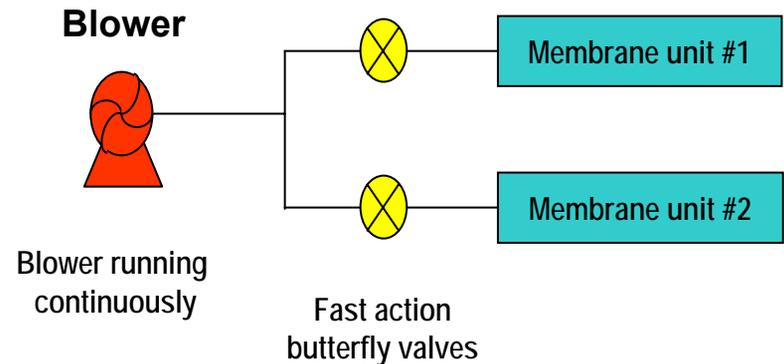
## • Biological process aeration

- Select MLSS to optimize OTE
  - Alpha factor decreases at higher MLSS
  - Limitation on OUR at higher MLSS
- Nit/DeNit recovers energy and alkalinity
- Fine bubble aeration in bioreactor

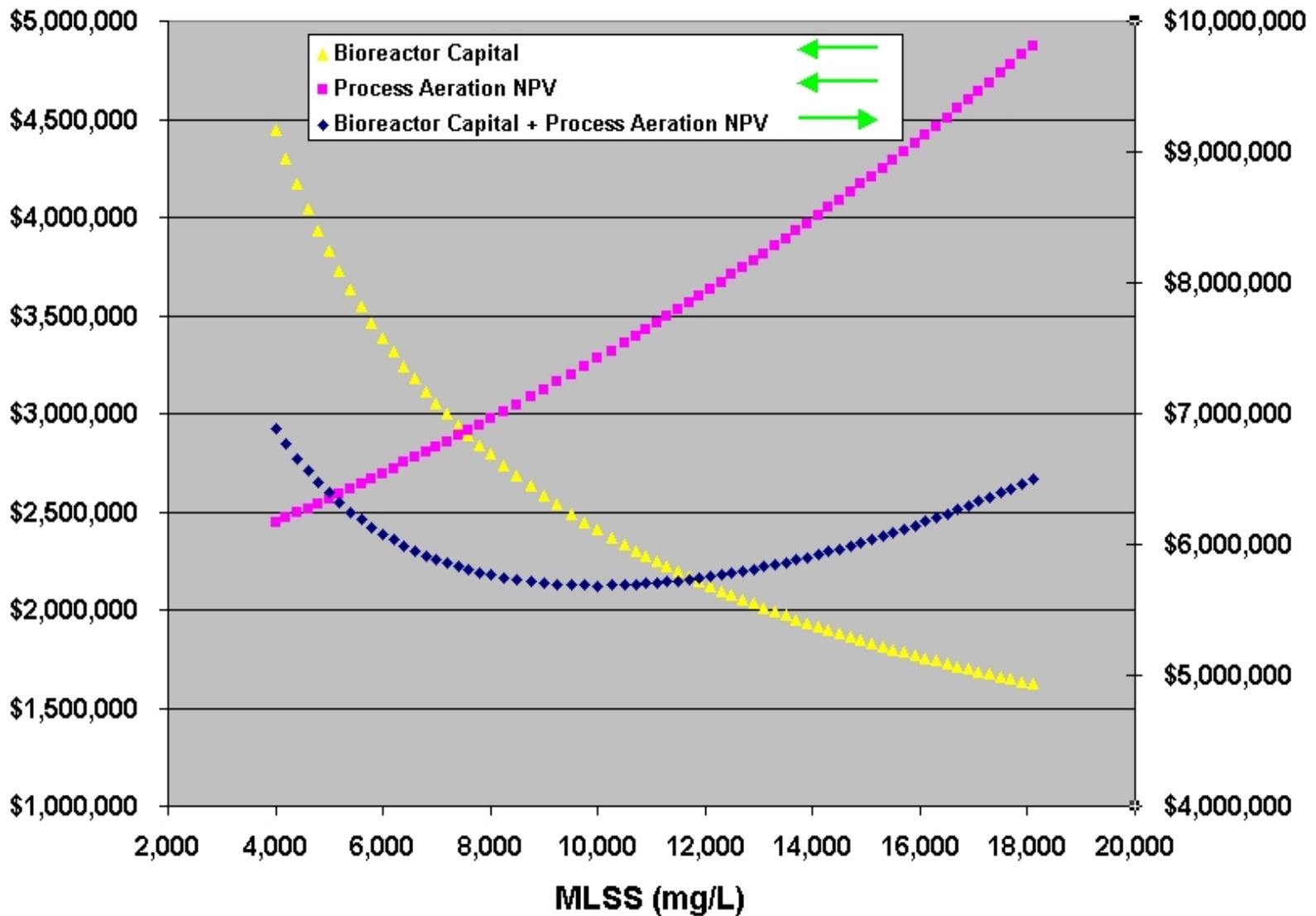


## • Membrane aeration

- Optimize membrane depth
- Cyclic aeration

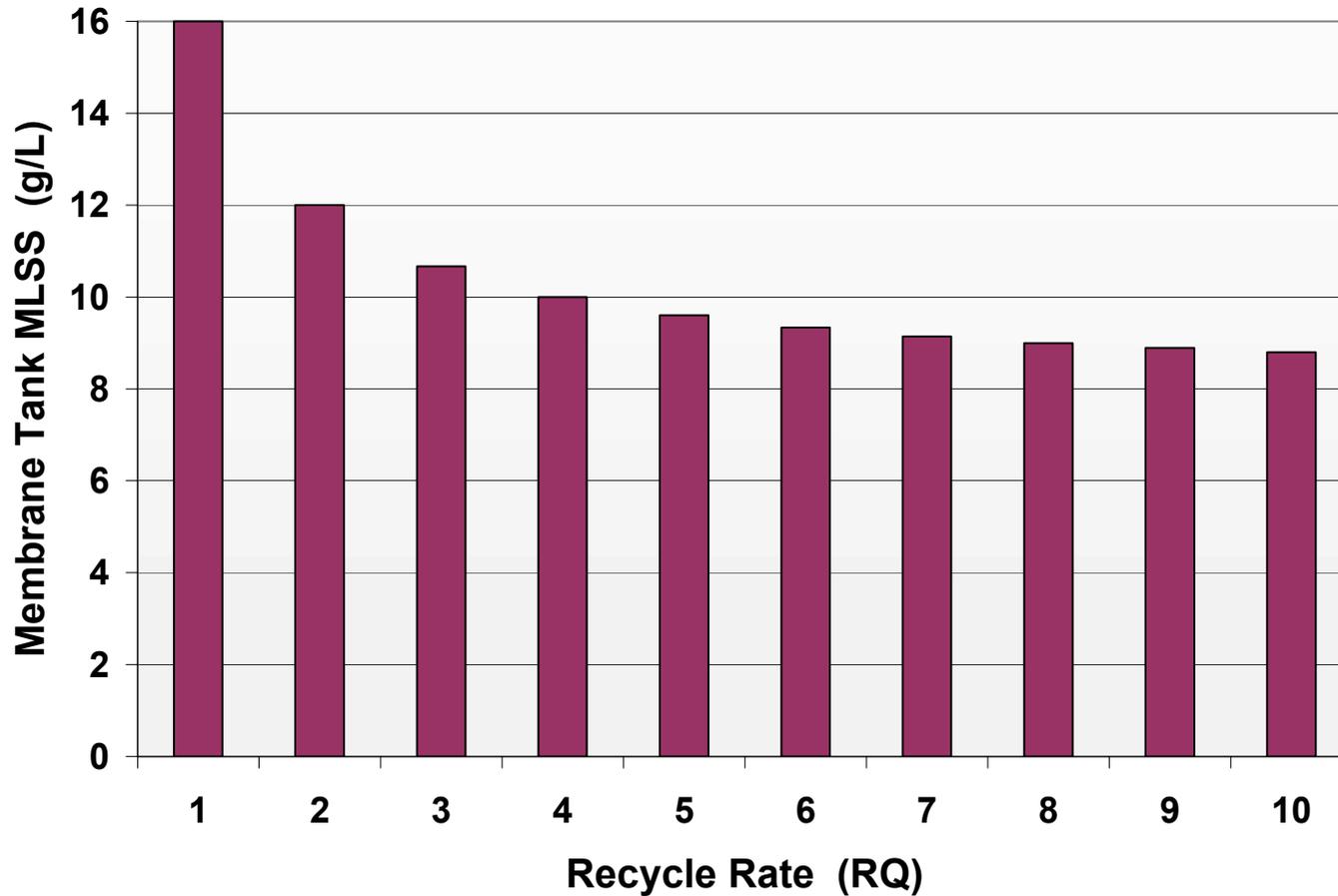


# Bio-Process NPV vs. MLSS Concentration



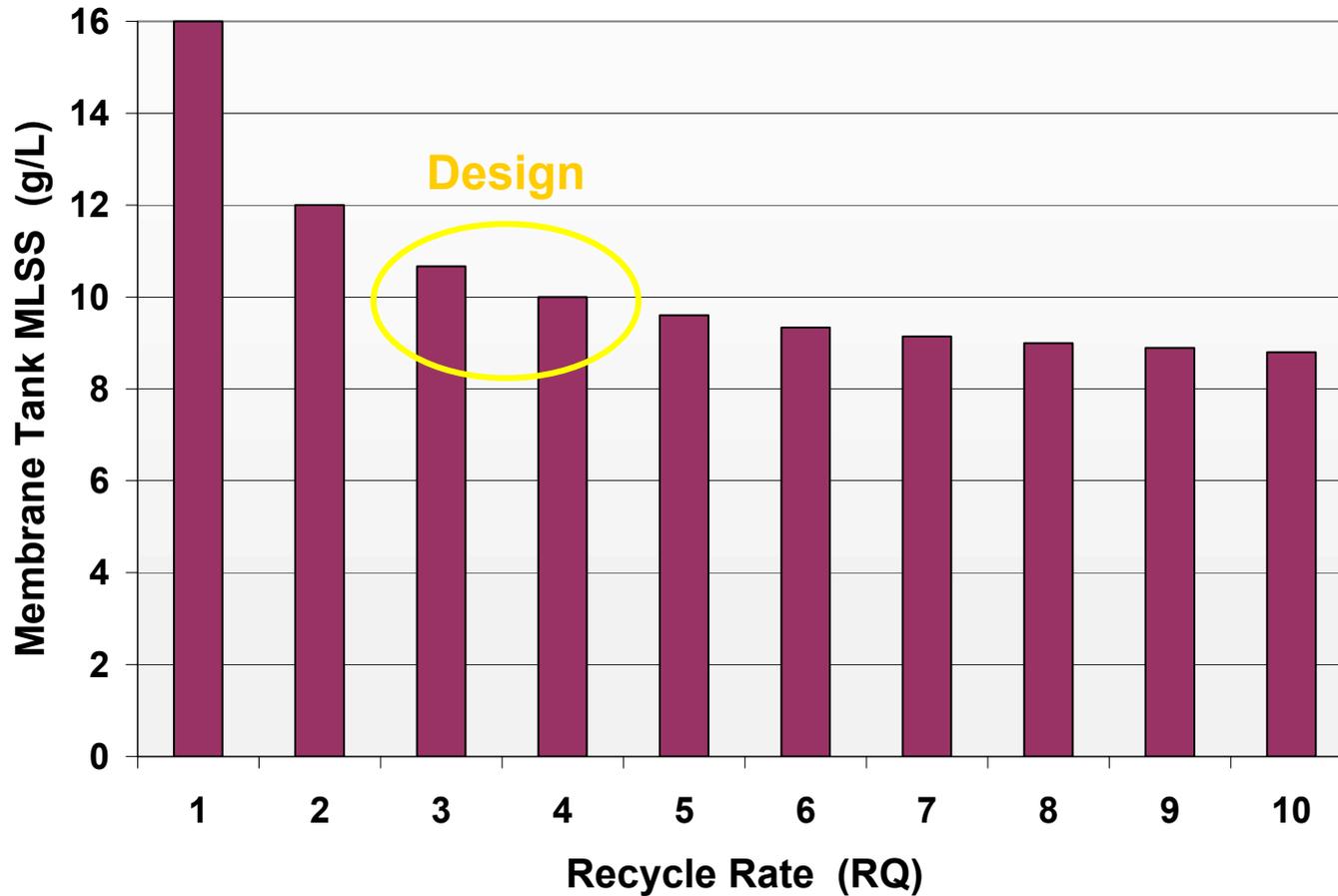
# MLSS Distribution

$$\text{MLSS}_{\text{membrane tank}} = \frac{(R+1)}{R} \times \text{MLSS}_{\text{bioreactor}}$$



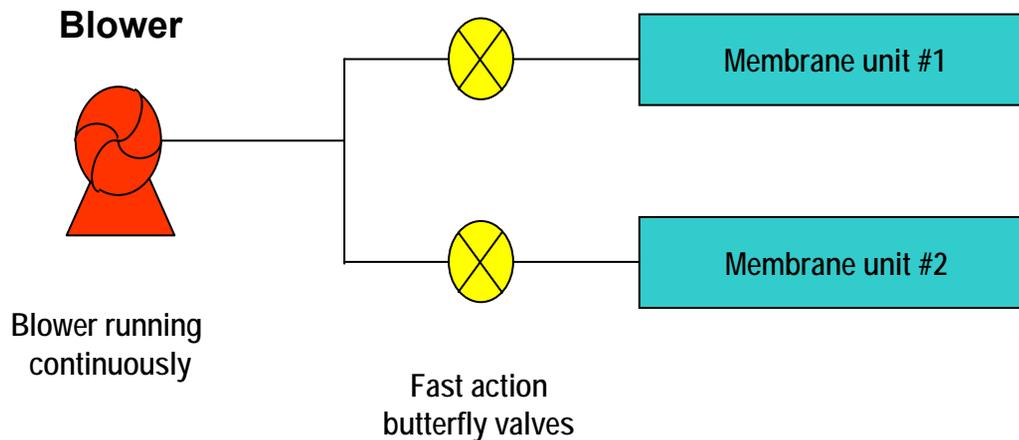
# MLSS Distribution

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# Membrane Aeration

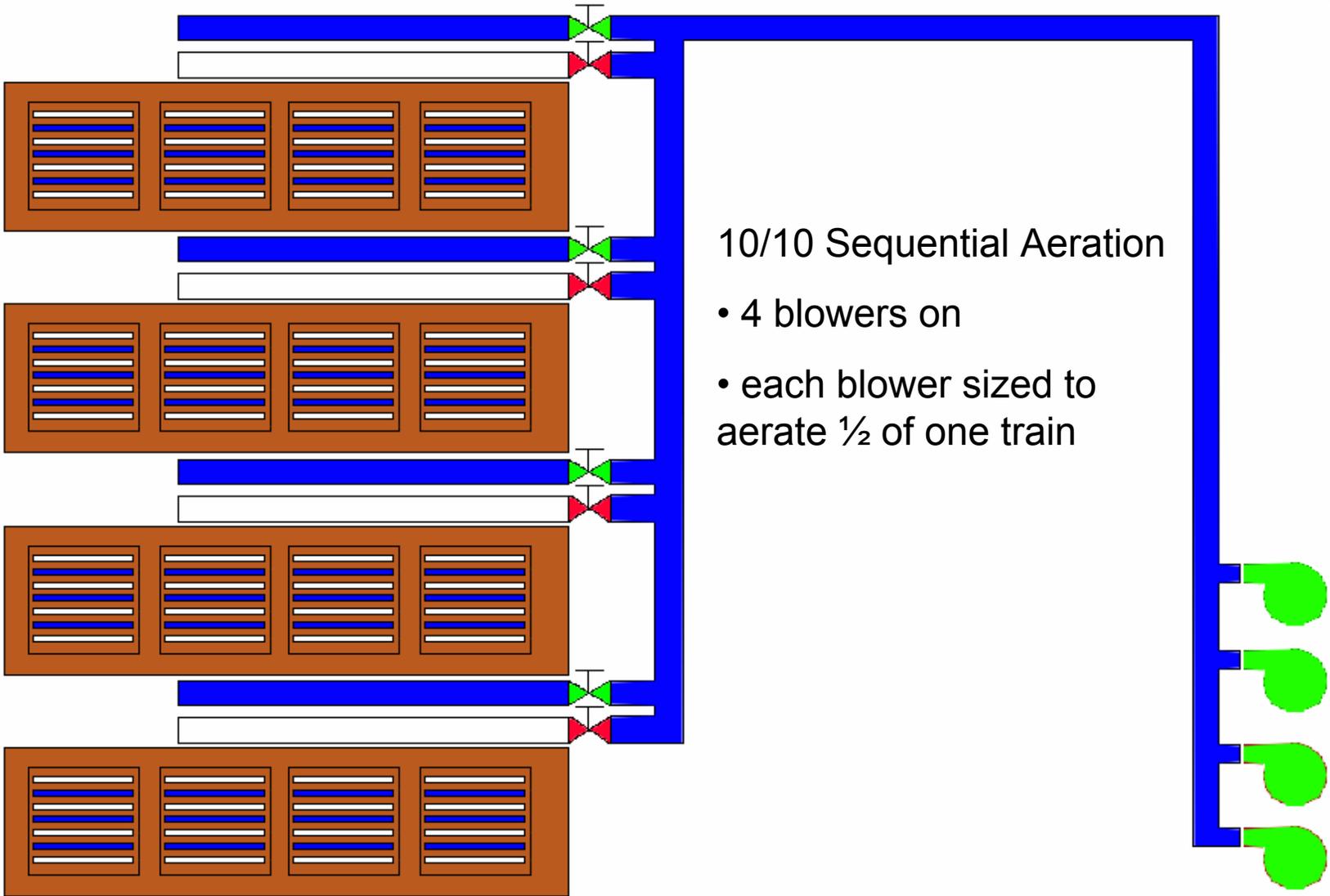
- Optimize membrane submergence to reduce blower discharge pressure
- Effective scouring with coarse bubble aeration
- Optimized cyclic aeration based on flow



US Patent 6,245,239

# 10/30 Aeration at ADF

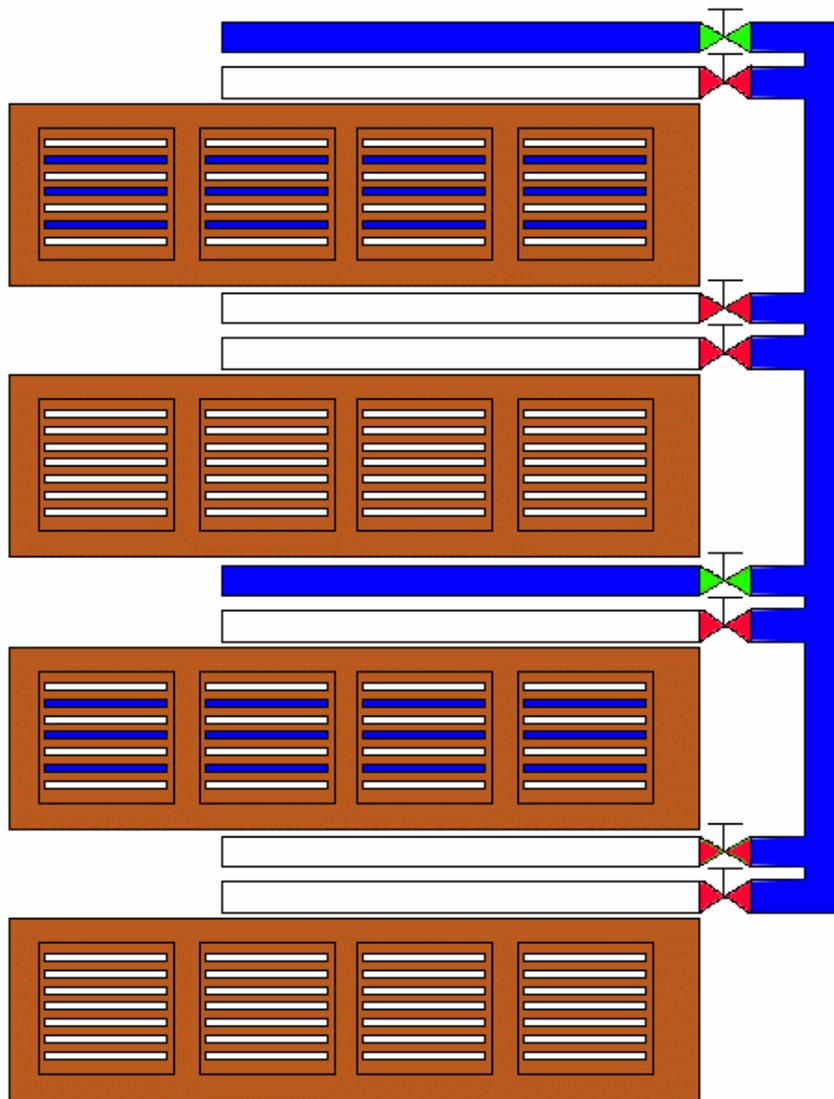
- Optimized cyclic aeration based on flow
- Maintain 10/10 Aeration at or above ADF
- Run at 10/30 Aeration below ADF
- 50% Savings compared to 10/10 = 7-10% LCC



### 10/10 Sequential Aeration

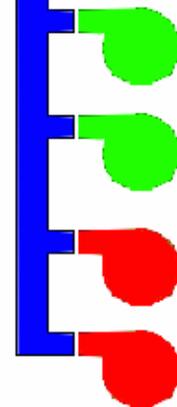
- 4 blowers on
- each blower sized to aerate  $\frac{1}{2}$  of one train

Note – Airflow is blue



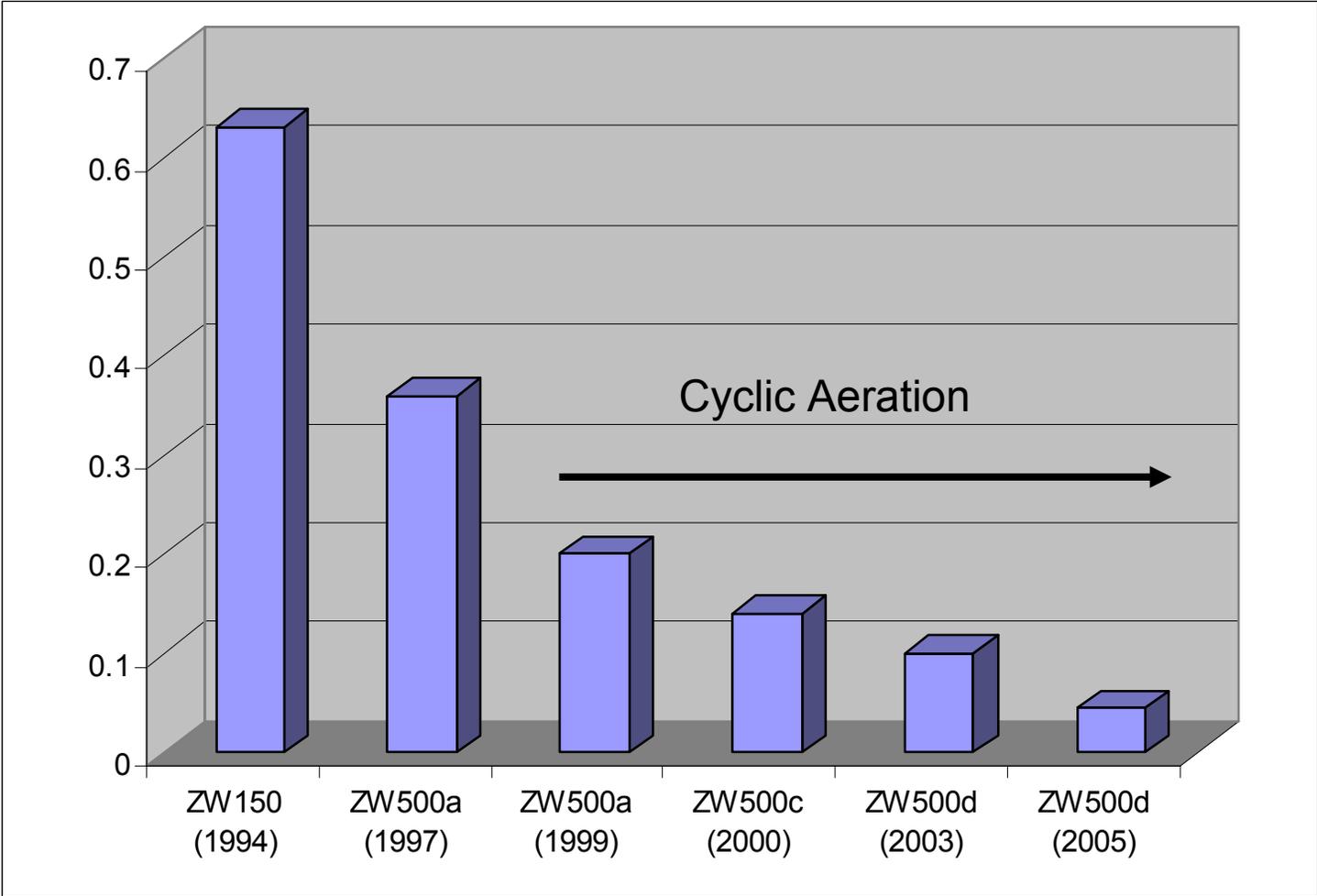
### 10/30 Sequential Aeration

- 2 blowers on
- each blower sized to aerate  $\frac{1}{2}$  of one train
- same instantaneous air flow rate as 10/10 BUT  $\frac{1}{2}$  the average



Note – Airflow is blue

# Evolution of ZeeWeed Membrane Aeration



# ZeeWeed® Cassette Scale-Up

Larger Cassettes = Lower Capital + O&M Costs



ZW-500a (1997)

4,000 ft<sup>2</sup>  
80,000 gpd



ZW-500c (2000)

5,500 ft<sup>2</sup>  
110,000 gpd



ZW-500d (2002)

16,300 ft<sup>2</sup>  
326,000 gpd



ZW-500d (2005)

21,800 ft<sup>2</sup>  
436,000 gpd

**Increasing Size**  
**Decreasing \$ / gal**

# Membrane Life and Warranty

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# Key Factors for Extended Membrane Life

- Select a robust membrane
- Protect the membrane
- Keep the membrane clean
- Design with a conservative flux
- Finite life time capacity

# Design Flux Selection

- Based on long-term, full-scale experience, rather than short-term data or pilot studies
- Design based on limiting hydraulic conditions
  - Maximum Flow
  - Minimum Temperature
  - Performance Beyond 5 Years
  - Minimum Safety Factor

Recommend Specifying  
Minimum Membrane Area **or** Maximum Peak Flux

# Life Time Membrane Capacity

Operating Flux [gfd]	5 yrs [gal/ft2]	8 yrs [gal/ft2]	10 yrs [gal/ft2]	15 yrs [gal/ft2]
5	9,125	14,600	18,250	27,375
10	18,250	29,200	36,500	54,750
15	27,375	43,800	54,750	82,125

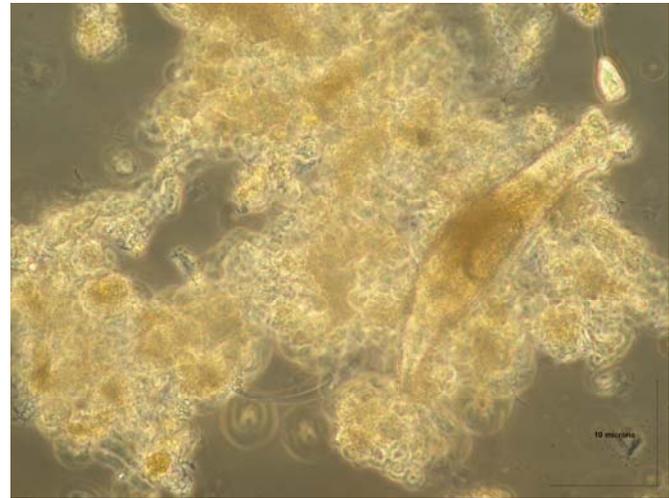
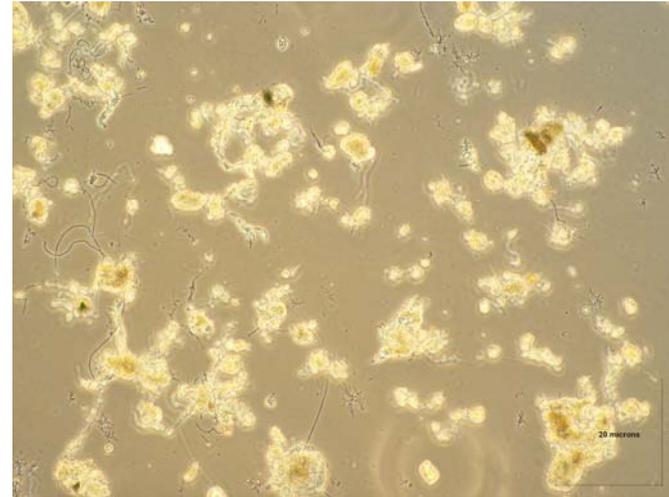
# Chemical Conditioning

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# Sludge Quality?

- Settleability not important
- Sludge Quality is a factor
- How do we measure?



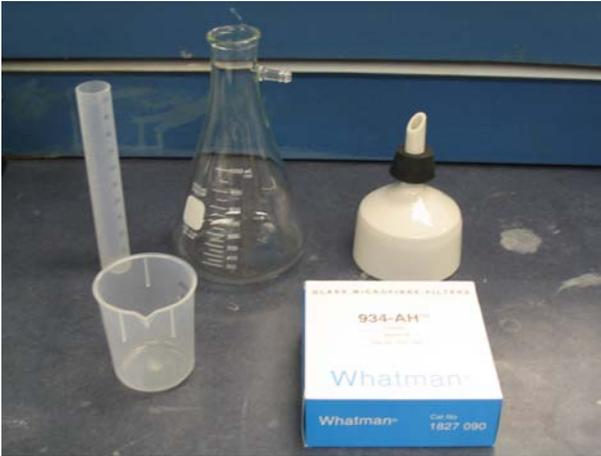
# Which of the following parameters are more important for MBR fouling

- TTF
- DSVI
- MLSS
- Specific cake resistance
- Silt density index (SDI)
- Fouling index (FI)
- Modified fouling index (MFI)
- Particle size distribution (>1.5  $\mu\text{m}$ )
- Colloidal TOC
- Soluble EPS
- Soluble carbohydrate
- Soluble protein
- Soluble humic acid
- Temperature
- Bound EPS
- Zeta-potential

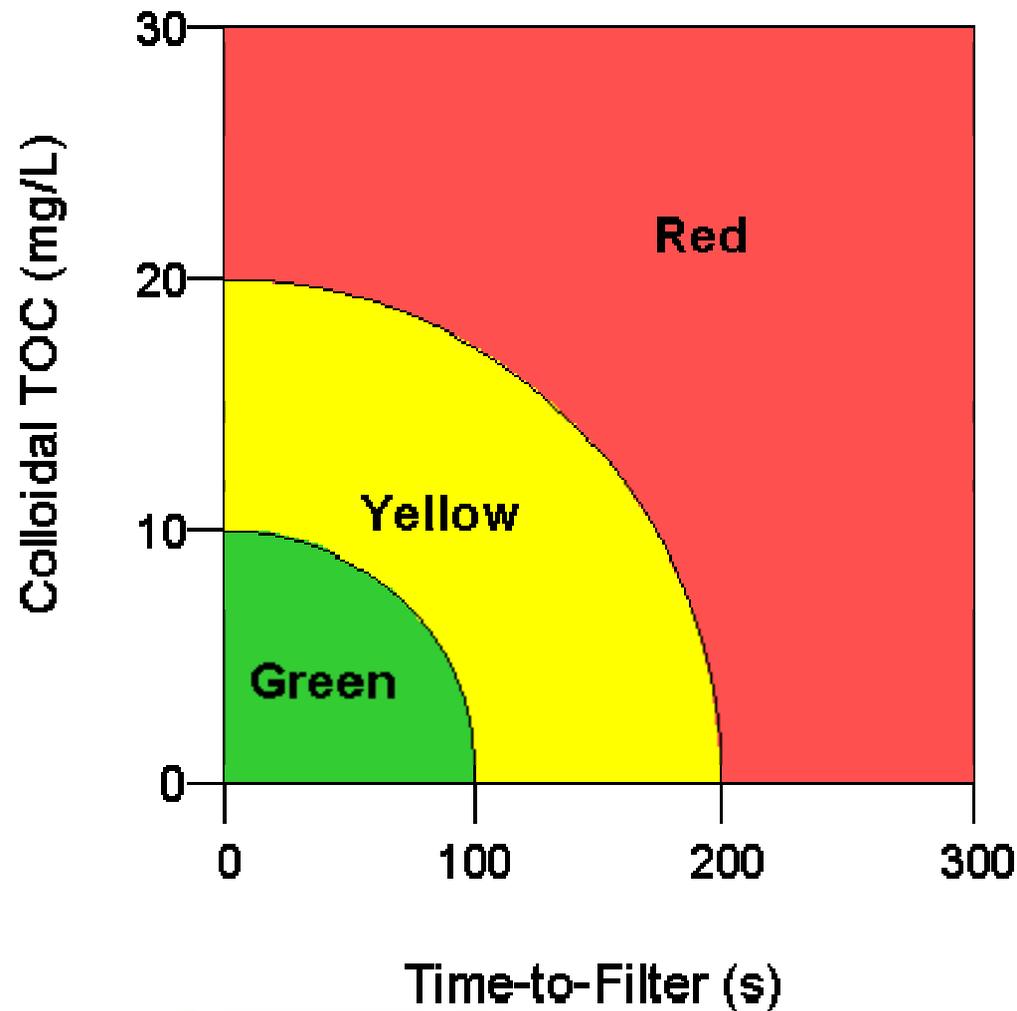
# Which of the following parameters are more important for MBR fouling

- **TTF**
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- Specific cake resistance
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- **Colloidal TOC**
- Soluble EPS
- Soluble carbohydrate
- Soluble protein
- Soluble humic acid
- Temperature
- Bound EPS
- Zeta-potential

# Sludge Quality - TTF

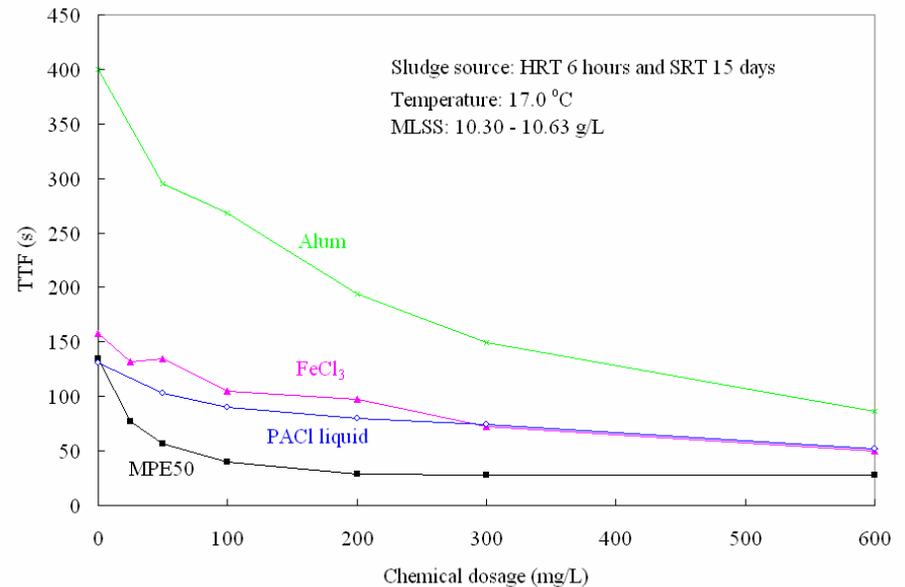


# Sludge Quality?



# Chemical Conditioning

- Coagulants, Polymers
- Significant Improvements
- Reliability
- Design Implementation

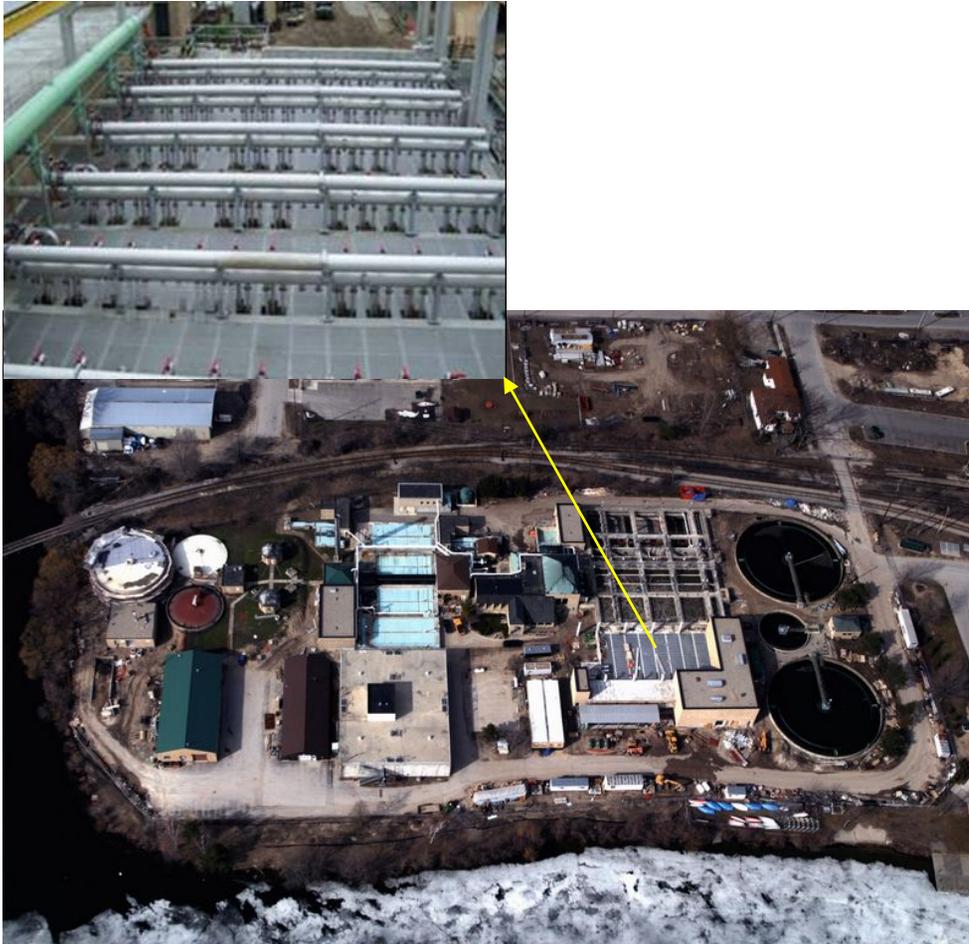


# New Projects

# Traverse City, MI

ADF: 7.1 MGD (26,500 m<sup>3</sup>/d)

Commission Date: **Summer 2004**



- Largest operating MBR based on peak flow
- Peak flow 17.2 mgd (65,000 m<sup>3</sup>/d)
- Primary Clarifier + Fine Screen
- 8 ZW500 trains
- Bio-P Removal

# Pooler, Georgia

ADF: 2.5 MGD (9,463 m<sup>3</sup>/d)



Commission Date: **November, 2004**

- Located near Savannah, GA
- 4 ZW500d trains with reversible pumps
- Simple, cost effective layout & construction
- Process optimization for flows < design

# F. Wayne Hill Water Resources Center

ADF: 47 MGD (177,914 m<sup>3</sup>/d)

Commission Date: **Summer 2005**



- Largest membrane tertiary filtration plant
- 16 ZW500 Trains
- Very strict effluent limits
  - Turbidity < 0.1 NTU
  - Particle Count < 10#/ml
- Discharges to Lake Lanier
  - Recreational and indirect potable reuse

# Jackson, Ohio

ADF: 2 MGD (7,571 m<sup>3</sup>/d)

Commission Date: 2006/2007

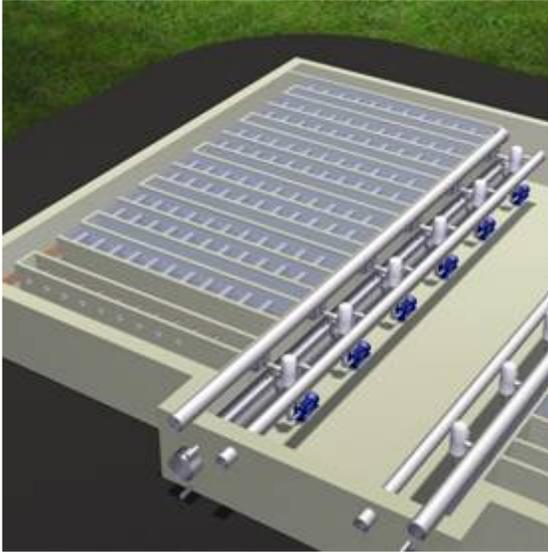


- Retrofit of old aeration tanks
- Will operate in parallel with existing ox ditches
- 4 trains, reversible pumps
- Zenon evaluated against other MBRs
- Selected based on experience and costs

# Brightwater WWTP

ADF: 31 MGD (117,347 m<sup>3</sup>/d)

Commission Date: **Expected 2009/10**



- World's Largest MBR awarded
- Phase 1 peak hour flow 44 mgd
- Phase 2 peak hour flow 57 mgd
- 10 trains at buildout
- 24 mgd of Class A Reclaimed Water
- Evaluated Bid



# Marco Island, Florida

ADF: 3 MGD (11,356 m<sup>3</sup>/d)

Commission Date: **June, 2006**



- Largest skid mounted system
- 5 mgd Peak Hour Flow
- 3+1 train - Fully redundant train (tank & skid)
- Skid includes:
  - Process pump
  - RAS pump
  - Membrane blower
  - PLC
  - MCC
  - All valves and wiring
- Negotiated

# Peoria, Arizona

ADF: 10 MGD (37,854 m<sup>3</sup>/d)

Commission Date: 2007



*Courtesy of B&V and City of Peoria*

- One of the fastest growing cities in the US
- Initial peak to 20 mgd
- Build-out to 13/26 mgd
- 10 membrane trains
- MBR evaluated against conventional
- Zenon evaluated against other MBRs
- Selected based on experience and costs

# Henderson South Wastewater Reclamation Facility

ADF: 8 MGD (30,283 m<sup>3</sup>/d)

Commission Date: July, 2009



- Fast growing community outside of Las Vegas
- Peak hour flow 13.6 mgd
- 8 membrane trains
- Evaluation based on defined lifecycle costs
- Zenon lowest LLC

Courtesy of CH2M Hill and City of Henderson

# Thank You!

Questions and Answers